

## Formula/Conversion Table for Water Treatment and Water Distribution

| Measurement Conversion      | Measurement Conversion | Measurement Conversion            | Measurement Conversion    |
|-----------------------------|------------------------|-----------------------------------|---------------------------|
| 1 ft. = 12 in.              | 1 MGD = 1.55 cfs       | 1 grain / gal = 17.1 mg/L         | 1 min = 60 sec            |
| 1 yd. = 3 ft.               | 1 cu. yd. = 27 cu. ft. | 1 gm = 1000 mg                    | 1 hour = 60 min           |
| 1 m = 3.28 ft.              | 1 cu. ft. = 7.48 gal   | 1 kg = 1000 gm                    | 1 day = 1440 min          |
| 1 mi = 5280 ft.             | 1 gal = 8.34 lbs       | 1 liter = 1000 ml                 | 1% = 10,000 mg/L          |
| 1 sq. ft. = 144 sq. in.     | 1 cu. ft. = 62.4 lbs   | 1 gal = 3.785L                    | 1 mg/l = 1 ppm            |
| 1 acre = 43,560 sq. ft.     | 1 kg = 2.2 lbs         | 1 psi = 2.31 ft. of water         | 1 hp= 0.746 kW            |
| 1 acre-ft. = 43,560 cu. ft. | 1 lb. = 454 gm         | 1 ft. water = 0.433 psi           | 1 hp = 33,000 ft. lbs/min |
| 1 acre-ft. = 325,829 gal    |                        | 1 in Mercury = 1.133 ft. of water | 1kW = 1,000 W             |

L = Length    B = Base    W = Width    H = Height    R = Radius    D = Diameter     $\pi = 3.14$

### Alkalinity

Phenolphthalein Alkalinity, as mg CaCO<sub>3</sub>/L =  $\frac{(\text{Titrant Volume A, ml})(\text{Acid Normality})(50,000)}{\text{Sample Volume, ml}}$

Total Alkalinity, as mg CaCO<sub>3</sub>/L =  $\frac{(\text{Titrant Volume B, ml})(\text{Acid Normality})(50,000)}{\text{Sample Volume, ml}}$

Alkalinity Relationships: Alkalinity, mg/l as CaCO<sub>3</sub>

| Result of Titration | Hydroxide Alkalinity as CaCO <sub>3</sub> | Carbonate Alkalinity as CaCO <sub>3</sub> | Bicarbonate Concentration as CaCO <sub>3</sub> |
|---------------------|---|---|--|
| P = 0               | 0   | 0   | T  |
| P < ½ T             | 0   | 2P  | T – 2P   |
| P = ½ T             | 0   | 2P  | 0  |
| P > ½ T             | 2P – T                                    | 2(T – P)                                  | 0  |
| P = T               | T   | 0   | 0  |

Key: P – phenolphthalein alkalinity; T – total alkalinity

### Area, Circumference and Volume

Area, sq ft

Circle:  $A = \pi \times R^2$  or  $A = 0.785 \times D^2$

Cylinder (total outside surface area):  $A = (2 \times \pi \times R^2) + \pi \times D \times H$  or  $A = (2 \times 0.785 \times D^2) + (\pi \times D \times H)$

Rectangle:  $A = L \times W$

Triangle:  $A = \frac{1}{2} \times B \times H$

Circumference, ft

Circle, ft =  $\pi \times D$

Rectangle, ft =  $2 \times L + 2 \times W$

Volume, cu ft:

Cone:  $V = \frac{1}{3} \times 0.785 \times D^2 \times H$  or  $V = \frac{1}{3} \times \pi \times R^2 \times H$

Cylinder:  $V = \pi \times R^2 \times H$  or  $V = 0.785 \times D^2 \times H$

Rectangle:  $V = L \times W \times H$

Average (arithmetic mean) =  $\frac{\text{Sum of All Terms or Measurements}}{\text{Number of Terms or Measurements}}$

Annual Running Average =  $\frac{\text{Sum of All Averages}}{\text{Number of Averages}}$

**Chemical Feed, Mixing and Solution Strengths**

$$\text{Chemical Feed, lbs/day} = \frac{(\text{Dry Chemical Collected, gm})(60 \text{ min/hr})(24 \text{ hr/day})}{(\text{Dry Chemical Feeder})(454 \text{ gm/lb})(\text{Time, min})}$$

$$\text{Chemical Feed, lbs/day} = \frac{(\text{Polymer Feeder}) \text{ Polymer Conc. mg/l}(\text{Volume Pumped, ml})(60 \text{ min/hr})(24 \text{ hr/day})}{(\text{Time Pumped, min})(1,000 \text{ mg/l})(1,000 \text{ mg/gm})(454 \text{ gm/lb})}$$

$$\text{Chemical Feed Pump Setting, \% Stroke} = \frac{(\text{Desired Flow})(100\%)}{\text{Maximum Flow}}$$

$$\text{Chemical Feed Pump Setting, mL/minute} = \frac{(\text{Flow, MGD})(\text{Dose, mg/L})(3.785 \text{ L/gal})(1,000,000 \text{ gal/MG})}{(\text{Liquid, mg/ml})(24 \text{ hr/day})(60 \text{ min/hr})}$$

$$\text{Chemical Flow, gpm} = \frac{\text{Volume Pumped, gal}}{(\text{Pumping Time, hr})(60 \text{ min/hr})}$$

$$\text{Dry Polymer, lbs} = (\text{Water, lbs}) / ((100 / \text{polymer \%}) - 1)$$

$$\text{Feeder Setting, \%} = \frac{(\text{Desired Feed Rate, lbs/day})(100\%)}{(\text{Maximum Feed Rate, lbs/day})} \quad \text{or} \quad \frac{(\text{Desired Feed Rate, gph})(100\%)}{\text{Maximum Feed Rate, gph}}$$

$$\text{Hypochlorite Strength, \%} = \frac{(\text{Chlorine Required, lbs})(100\%)}{(\text{Hypochlorite Solution Needed, gal})(8.34 \text{ lbs/gal})}$$

$$\text{Liquid Polymer, gal} = \frac{(\text{Polymer Solution, \%})(\text{gal of solution})}{\text{Liquid Polymer, \%}}$$

$$\text{Mixture Strength, \%} = \frac{(\text{Amount 1, gals})(\text{Strength 1, \%}) + (\text{Amount 2, gals})(\text{strength 2, \%})}{(\text{Amount 1, gals}) + (\text{Amount 2, gals})}$$

$$\text{Polymer Strength, \%} = \frac{(\text{Dry Polymer, lbs})(100\%)}{(\text{Dry Polymer, lbs} + \text{Water, lbs})} \quad \text{or} \quad \frac{(\text{Weight of Solute, lbs})(100\%)}{\text{Weight of Solution}}$$

$$\text{Water, lbs} = \frac{(\text{Dry Polymer, lbs})(100\%) - \text{Dry polymer, lbs}}{\text{Polymer \%}}$$

$$\text{Water added, gal} = \frac{(\text{hypo, gal})(\text{hypo, \%}) - (\text{hypo, gal})(\text{desired hypo, \%})}{\text{Desired hypo, \%}}$$

**Demineralization**

$$\text{Membrane Area, sq ft} = (\text{Number of Vessels})(\text{Number of Elements/Vessel})(\text{Surface Area/Element})$$

$$\text{Average Flux Rate, GFD} = \frac{\text{Permeate Flow, gpd}}{\text{Membrane Area, sq ft}}$$

$$\text{Mineral Rejection, \%} = \left[ 1 - \frac{\text{Product Concentration (TDS), mg/l}}{\text{Feedwater Concentration (TDS), mg/l}} \right] \times 100\%$$

$$\text{Recovery, \%} = \frac{(\text{Product Flow, mgd})(100\%)}{(\text{Feed Flow, mgd})}$$

**Detention Time**

$$\text{Detention Time (days)} = \frac{\text{Volume, gallons}}{\text{Flow, gpd}} \quad \text{Note: For detention time in hours multiply by 24hr/day and for detention time in minutes multiply by 1440 min/day}$$

**Disinfection**

Chlorine Demand, mg/L = Chlorine Dosage, mg/L – Chlorine Residual, mg/L

Chlorine Dosage, mg/L = Chlorine Demand, mg/L + Chlorine Residual, mg/L

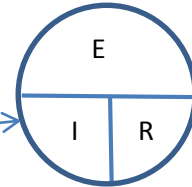
Chlorine Residual, mg/L = Chlorine Dosage, mg/L – Chlorine Demand, mg/L

CT calculation, time = (Disinfectant Residual Concentration, mg/L)(Time) Units must be compatible

**Electrical**

Amps (I) =  $\frac{\text{Volts (E)}}{\text{Ohms (R)}}$

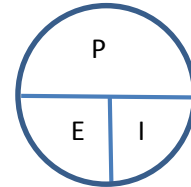
Electromotive Force (E.M.F.), volts = (Current, amps)(Resistance, ohms) or  $E = I \times R$



Power, kilowatts (3 phase AC circuit) =  $\frac{(\text{E, volts})(\text{I, amps})(\text{Power Factor})(1.73)}{1,000 \text{ watts/kilowatt}}$

Power, kilowatts (single phase AC circuit) =  $\frac{(\text{E, volts})(\text{I, amps})(\text{Power Factor})}{1,000 \text{ watts/kilowatt}}$

Power, watts (DC circuit) = (E, volts)(I, amps) or  $P = E \times I$

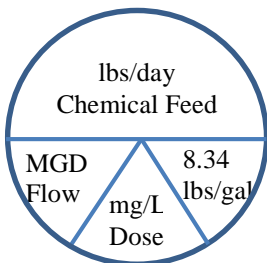


Power Output, horsepower =  $\frac{(\text{Power Input, kilowatts})(\text{Efficiency, \%})}{(0.746 \text{ kilowatt/horsepower})(100\%)}$

Power Requirements, kW-hr = (Power, kilowatts)(Time, hours)

**Feed Rate**

Feed Rate, lbs/day =  $\frac{(\text{Dosage, mg/L})(\text{Flow, MGD})(8.34 \text{ lbs/gal})}{(\text{Purity, as a decimal})}$



Davidson Pie Chart

- To find the quantity above the horizontal line: multiply the pie wedges below the line together and divide by the purity, as a decimal (i.e., 65% = 0.65).
- To solve for one of the pie wedges below the horizontal line: cover that pie wedge then divide the remaining pie wedges into the quantity above the horizontal line and multiply by the purity, as a decimal (i.e., 65% = 0.65).
- The given units must match the units shown in the pie wheel.

**Filtration**

Backwash Rise Rate, in/min =  $\frac{(\text{Backwash Rate, gpm/sq. ft.})(12 \text{ in/ft})}{(7.48 \text{ gal/cu. ft.})}$

Backwash Pumping Rate, gal/min = (Backwash Rate, gpm/sq. ft.)(Filter Surface Area, sq. ft.)

Backwash Water Required, gal = (Backwash Flow, gpm)(Backwash Time, min)

Backwash Water Used, % =  $\frac{(\text{Backwash Water, gal})(100\%)}{\text{Water Filtered, gal.}}$

Drop Velocity (V), ft/min =  $\frac{\text{Water Drop in Filter, ft}}{\text{Time to Drop, min}}$

Filtration Rate or Backwash Rate, GPM/sq. ft. =  $\frac{\text{Flow, GPM}}{\text{Filter Surface Area, sq. ft.}}$

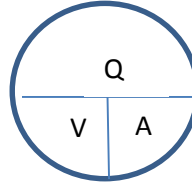
$$\text{Hydraulic or Surface Loading Rate, gpd/sq ft} = \frac{\text{Total Flow Applied, gpd}}{\text{Surface Area, sq ft}}$$

$$\text{Unit Filter Run Volume, gal/sq. ft.} = \frac{\text{Volume Filtered, gal}}{\text{Filter Surface Area, sq. ft.}}$$

$$\text{Unit Filter Run Volume, gal/sq. ft.} = (\text{Filtration Rate, GPM/sq. ft.})(\text{Filter Run, hr})(60 \text{ min/hr})$$

### **Flow Rates and Velocity** (pipe line, channel or stream)

$$\text{Flow Rate, cfs} = (\text{Area, sq. ft.})(\text{Velocity, ft/sec}) \text{ or } Q = V \times A$$



Where:  
 Q = flow rate, cfs  
 V = velocity, fps  
 A = area, ft<sup>2</sup>

$$\text{Flow Rate, gpm} = (\text{Area, sq. ft.})(\text{Velocity, ft/sec})(7.48 \text{ gal/cu ft})(60 \text{ sec/min}) \text{ or } Q = V \times A \times 7.48 \times 60$$

$$\text{Velocity, fps} = \frac{\text{Flow rate, cfs}}{\text{Area, sq ft}} \text{ or } \frac{\text{Distance, ft}}{\text{Time, seconds}}$$

$$\text{Reduction in Flow, \%} = \frac{(\text{Original Flow} - \text{Reduced Flow})(100\%)}{\text{Original Flow}}$$

### **Fluoridation**

$$\text{Feed Rate, lbs/day} = \frac{(\text{Dosage, mg/L})(\text{Flow, MGD})(8.34 \text{ lbs/gal})}{(\text{Fluoride solution, as a decimal})(\text{Purity, as a decimal})}$$

$$\text{Feed Rate, gpd} = \frac{\text{Feed Rate, lbs/day}}{\text{Chemical solution, lbs/gal}}$$

$$\text{Feed Rate, lbs/day} = \frac{\text{Fluoride, lbs/day}}{\text{Fluoride, lbs / lb of commercial chemical}}$$

$$\text{Fluoride ion purity, \%} = \frac{(\text{Molecular Weight of Fluoride})(100\%)}{\text{Molecular Weight of Compound}}$$

$$\text{Portion of Fluoride} = \frac{(\text{Commercial Chemical Purity, \%})(\text{Fluoride ion, \%})}{(100\%) (100\%)}$$

### **Flushing Time**

$$\text{Flushing Time, sec} = \frac{\text{Volume, cu ft}}{\text{Flow, cfs}} \text{ or } \frac{(\text{Length of Pipeline, ft})(\text{Number of Flushing Volumes})}{(\text{Velocity, ft/sec})}$$

### **Laboratory**

$$\text{Dilute to ml} = \frac{(\text{Actual Weight, gm})(1,000 \text{ ml})}{(\text{desired Weight, gm})}$$

$$\text{Langelier Index (L.I.)} = \text{pH} - \text{pHs}$$

**Leakage and Pressure Testing Pipelines**

$$\text{Leakage, gpd} = \frac{\text{Volume, gal}}{\text{Time, days}}$$

$$\text{AC or Ductile Iron Pipe, gpd/mi-in} = \frac{\text{Leak Rate, gpd}}{(\text{length, mi})(\text{Diameter, in})}$$

$$\text{Plastic pipe, gph/100 joints} = \frac{\text{Leak Rate, gph}}{(\text{Number of Joints}) / (100 \text{ Joints})}$$

$$\text{Test Pressure, psi} = \text{Normal Pressure} + 50\% \text{ or } 150\text{psi whichever is greater}$$

**Loading**

$$\text{Weir Overflow Rate, gpd/ft} = \frac{\text{Total Flow, gpd}}{\text{Length of Weir, ft}}$$

**Parts per million**

$$\text{ppm} = \text{mg/l} = \frac{\text{Pounds of Chemical, lbs}}{(8.34 \text{ lbs/gal})(\text{gallons, MG})}$$

**Pressure and Head**

$$\text{Head (Height of Water), ft} = (\text{Pressure, psi})(2.31 \text{ ft / psi}) \quad \text{or} \quad \text{Head (Height of Water)} = \frac{\text{Pressure, psi}}{0.433 \text{ psi/ft}}$$

$$\text{Pressure, psi} = \frac{\text{Height, ft}}{2.31 \text{ ft/psi}} \quad \text{or} \quad \text{Pressure, psi} = \text{Height, ft} \times 0.433 \text{ psi/ft}$$

**Pumps and Motors**

$$\text{Brake (bhp)} = \frac{(\text{Flow, GPM})(\text{Head, ft})}{(3,960)(\text{Decimal Pump Efficiency})}$$

$$\text{Motor (mhp)} = \frac{(\text{Flow, GPM})(\text{Head, ft})}{(3,960)(\text{Decimal Pump Efficiency})(\text{Decimal Motor Efficiency})}$$

$$\text{Water (whp)} = \frac{(\text{Flow, GPM})(\text{Head, ft})}{3,960}$$

$$\text{Pumping Rate, GPM} = \frac{\text{Volume, gal}}{\text{Time, min}}$$

$$\text{Total Dynamic Head, ft} = \text{Static Head, ft} + \text{Discharge Head, ft} + \text{Friction Losses, ft}$$

$$\text{Wire-to-Water Efficiency, \%} = \frac{(\text{Water Horsepower, HP})(100\%)}{\text{Power Input, (Brake HP or Motor HP)}}$$

$$\text{Wire-to-Water Efficiency, \%} = \frac{(\text{Flow, gpm})(\text{Total Dynamic Head, ft})(100\%)}{(\text{Voltage, volts})(\text{Current, amps})(5.308)}$$

$$\text{Kilowatt- hr/day} = (\text{Motor, HP}) \frac{\times 24 \text{ hr}}{\text{day}} \times \frac{0.746 \text{ kW}}{\text{HP}}$$

$$\text{Cost, \$/day} = \text{Kilowatt-hr/day} \times \text{cost, \$/kWh}$$

**Softening Processes****Hardness**

$$\begin{aligned} \text{Total Hardness, mg/l as CaCO}_3 &= \text{Calcium Hardness, mg/l as CaCO}_3 + \text{Magnesium Hardness, mg/l as CaCO}_3 \\ &= (2.5)(\text{Ca, mg/l}) + (4.12)(\text{Mg, mg/l}) \end{aligned}$$

If alkalinity is greater than total hardness:

$$\begin{aligned} \text{Carbonate Hardness, mg/l as CaCO}_3 &= \text{Total Hardness, mg/l as CaCO}_3 \text{ and} \\ \text{Noncarbonate Hardness, mg/l as CaCO}_3 &= 0 \end{aligned}$$

If alkalinity is less than total hardness:

$$\begin{aligned} \text{Carbonate Hardness, mg/l as CaCO}_3 &= \text{Alkalinity, mg/l as CaCO}_3 \text{ and} \\ \text{Noncarbonate Hardness, mg/l as CaCO}_3 &= \text{Total Hardness} - \text{Alkalinity removed, mg/l as CaCO}_3 \end{aligned}$$

**Lime Softening** - If hydrated lime ( $\text{Ca(OH)}_2$ ) is used instead of quicklime ( $\text{CaO}$ ), substitute 74 for 56 in equations below.

$$\text{Lime Feed, mg/l} = \frac{(\text{A} + \text{B} + \text{C} + \text{D}) \times 1.15}{\text{Purity of Lime, as a decimal}}$$

$$\begin{aligned} \text{A} &= \text{Carbon dioxide (CO}_2\text{) in source water:} && \text{mg/l as CO}_2 && \times (56/44) \\ \text{B} &= \text{Bicarbonate alkalinity removed in softening:} && \text{source water, mg/l as CaCO}_3 - \text{softened water, mg/l as CaCO}_3 && \times (56/100) \\ \text{C} &= \text{Hydroxide alkalinity in softener effluent:} && \text{mg/l as CaCO}_3 && \times (56/100) \\ \text{D} &= \text{Magnesium removed in softening:} && \text{source water, mg/l as Mg}^{2+} - \text{softened water, mg/l as Mg}^{2+} && \times (56/24.3) \end{aligned}$$

$$\text{Excess Lime, mg/l} = (\text{A} + \text{B} + \text{C} + \text{D})(0.15)$$

Soda Ash: dosage to remove noncarbonated hardness

$$\text{Soda Ash (Na}_2\text{CO}_3\text{) Feed, mg/l} = (\text{Noncarbonate Hardness, mg/l as CaCO}_3)(106/100)$$

Carbon Dioxide: dosage to recarbonate

$$\text{Total CO}_2\text{ Feed, mg/l} = (\text{excess lime, mg/l})(44/56) + (\text{Mg}^{2+}\text{ residual, mg/l})(44/58.3)$$

$$\text{Feeder Setting, lbs/day} = (\text{Flow, MGD})(\text{Dose, mg/l})(8.34 \text{ lbs/gal})$$

$$\text{Feed Rate, lbs/min} = \frac{\text{Feeder Setting, lbs/day}}{(60 \text{ min/hr})(24 \text{ hr/day})}$$

**Ion Exchange Softening**

$$\text{Hardness, grains/gallon} = \frac{(\text{Hardness, mg/l})(1 \text{ grain/gallon})}{17.1 \text{ mg/l}}$$

$$\text{Exchange Capacity, grains} = (\text{Media Volume, cu ft})(\text{Removal Capacity, grains/cu ft})$$

$$\text{Water Treated, gal} = \frac{\text{Exchange Capacity, grains}}{\text{Hardness Removed, grains/gallon}}$$

$$\text{Operating Time, hr} = \frac{\text{Water Treated, gal}}{(\text{Avg Daily Flow, gpm})(60 \text{ min/hr})}$$

$$\text{Salt Needed for Regeneration, lbs} = \text{Salt Required, lbs/1,000 grains}(\text{Hardness Removed, grains})$$

$$\text{Brine, gal} = \frac{\text{Salt Needed, lbs}}{\text{Salt Solution, lbs/gal of brine}}$$

$$\text{Bypass Flow, gpd} = \frac{(\text{Total Flow, gpd})(\text{Finished Water Hardness, gpg})}{\text{Source Water Hardness, gpg}}$$

$$\text{Bypass Water, gal} = \frac{(\text{Softener Capacity, gal})(\text{Bypass Flow, gpd})}{\text{Softener Flow, gpd}}$$

$$\text{Total Flow, gal} = \text{Softener Capacity, gal} + \text{Bypass Water, gal}$$

**Temperature**

$$\text{Degrees Celsius} = [(\text{°F} - 32)(\frac{5}{9})] \text{ or } [(\text{°F} - 32)(0.555)] \text{ or } \frac{(\text{°F} - 32)}{1.8}$$

$$\text{Degrees Fahrenheit} = [(\text{°C})(\frac{9}{5}) + 32] \text{ or } [(\text{°C})(1.8) + 32]$$

**Turbidity**

$$\text{Removal Percentage, \%} = \frac{(\text{Influent Turbidity} - \text{Effluent Turbidity})(100\%)}{\text{Influent Turbidity}}$$

**Water Production**

$$\text{Gallons/Capita/Day} = \frac{\text{Volume of Water Produced, gpd}}{\text{Population}}$$

***Abbreviations:***

| Abbreviations | Types of Measurement            | Abbreviations | Measurement Volumes     |
|---------------|---------------------------------|---------------|-------------------------|
| cfs           | Cubic feet per second           | m             | Meter                   |
| DO            | Dissolved oxygen                | mg            | Milligrams              |
| ft            | Feet                            | mg/L          | Milligrams per liter    |
| fps           | Feet per second                 | lbs           | Pounds                  |
| GFD           | Gallons per day per square foot | MGD           | Million gallons per day |
| gm            | Grams                           | mL            | Milliliter              |
| gpd           | Gallons per day                 | ppb           | Parts per billion       |
| gpg           | Grains per gallon               | ppm           | Parts per million       |
| gpm           | Gallons per minute              | psi           | Pounds per square inch  |
| gph           | Gallons per hour                | Q             | Flow                    |
| gr            | Grains                          | SS            | Settleable solids       |
| hp            | Horsepower                      | TTHM          | Total trihalomethanes   |
| in            | Inch                            | TOC           | Total organic carbon    |
| kg            | Kilogram                        | TSS           | Total suspended solids  |
| kW            | Kilowatt                        | VS            | Volatile solids         |
| kWh           | Kilowatt-hour                   | W             | Watt                    |